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APPLICATION NO.	FILING DATE	FIRST NAMED INVENTOR	ATTORNEY DOCKET NO.	CONFIRMATION NO.	
09/782,753	02/13/2001	William John Gauthier	31223-71413 9693		
7	590 05/21/2003				
Fina Technology Inc Attn Lenora Evans P O Box 674412			EXAMINER		
			BROWN, JENNINE M		
Houston, TX	77267-4412		ART UNIT	PAPER NUMBER	
	1755				
			DATE MAILED: 05/21/2003		

Please find below and/or attached an Office communication concerning this application or proceeding.

					<u> </u>
		Applicati	nN.	Applicant(s)	
		09/782,7	53	GAUTHIER ET AL.	
Office Action Summary		Examine	7	Art Unit	
		Jennine N	= . =	1755	
Peri d f	The MAILING DATE f this communi r Reply	ication appears on th	e cover sheet	with the correspondence address	
THE I - Exter after - If the - If NO - Failu - Any r	ORTENED STATUTORY PERIOD FOMALLING DATE OF THIS COMMUNIONS of time may be available under the provisions SIX (6) MONTHS from the mailing date of this common period for reply specified above is less than thirty (30 period for reply is specified above, the maximum state to reply within the set or extended period for reply seply received by the Office later than three months and dipatent term adjustment. See 37 CFR 1.704(b).	CATION. of 37 CFR 1.136(a). In no extraction. D) days, a reply within the statutory period will apply and will, by statute, cause the app	rent, however, may tutory minimum of t rill expire SIX (6) Mo blication to become	a reply be timely filed nirty (30) days will be considered timely. DNTHS from the mailing date of this communicati ABANDONED (35 U.S.C. § 133).	ion.
1)	Responsive to communication(s) file	ed on			
2a) <u></u>	This action is FINAL .	2b)⊠ This action is	non-final.		
3)□ Disp siti	Since this application is in condition closed in accordance with the praction of Claims				s is
4)⊠	Claim(s) 1-34 is/are pending in the a	application.			
	4a) Of the above claim(s) is/ar	re withdrawn from co	nsideration.		
5)	Claim(s) is/are allowed.				
6)⊠	Claim(s) <u>1-34</u> is/are rejected.				
	Claim(s) is/are objected to.				
· · · · · ·	Claim(s) are subject to restrict	tion and/or election r	eguirement.		
	on Papers		•		
9) 🗌 -	The specification is objected to by the	e Examiner.			
10) 🔲 -	The drawing(s) filed on is/are:	a) accepted or b)	objected to by	the Examiner.	
	Applicant may not request that any obje	ection to the drawing(s	be held in abe	yance. See 37 CFR 1.85(a).	
11) 🔲 🗆	he proposed drawing correction filed	l on is: a)∏ a	pproved b)	disapproved by the Examiner.	
	If approved, corrected drawings are req	quired in reply to this O	ffice action.		
12) 🔲 🖺	he oath or declaration is objected to	by the Examiner.			
Priority u	nder 35 U.S.C. §§ 119 and 120				
13)	Acknowledgment is made of a claim	for foreign priority ur	nder 35 U.S.C	. § 119(a)-(d) or (f).	
a)[☐ All b)☐ Some * c)☐ None of:				
	1. Certified copies of the priority of	documents have bee	n received.		
	2. Certified copies of the priority of	documents have bee	n received in	Application No	
	 Copies of the certified copies of application from the Internated the attached detailed Office action 	ational Bureau (PCT	Rule 17.2(a))		
14) 🔲 A	cknowledgment is made of a claim fo	or domestic priority u	nder 35 U.S.C	c. § 119(e) (to a provisional applica	tion).
	☐ The translation of the foreign land		•		
Attachment	(s)				
2) Notice	e of References Cited (PTO-892) e of Draftsperson's Patent Drawing Review (PT nation Disclosure Statement(s) (PTO-1449) Pa			v Summary (PTO-413) Paper No(s) f Informal Patent Application (PTO-152)	.•
D.S. Patent and Tr PTO-326 (Re		Office Acti n Summa	ry	Part of Paper No. 7	-

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DETAILED ACTION

Abstract

Applicant is reminded of the proper language and format for an abstract of the disclosure.

The abstract should be in narrative form and generally limited to a single paragraph on a separate sheet within the range of 50 to 150 words. It is important that the abstract not exceed 150 words in length since the space provided for the abstract on the computer tape used by the printer is limited. The form and legal phraseology often used in patent claims, such as "means" and "said," should be avoided. The abstract should describe the disclosure sufficiently to assist readers in deciding whether there is a need for consulting the full patent text for details.

The language should be clear and concise and should not repeat information given in the title. It should avoid using phrases which can be implied, such as, "The disclosure concerns," "The disclosure defined by this invention," "The disclosure describes," etc.

Claim Objections

Claims 5, 18, 19, 20, 21, 22 and 29 are objected to because of the following informalities: Each of the claims uses an inconsistent preamble terminology. The primary claims refer to "a process" and the subsequent dependent claims cited by Examiner refer to "a method". Appropriate correction is required.

Claim Rejections - 35 USC § 102

(e) the invention was described in (1) an application for patent, published under section 122(b), by another filed in the United States before the invention by the applicant for patent or (2) a patent granted on an application for patent by another filed in the United States before the invention by the applicant for patent, except that an international application filed under the treaty defined in section 351(a) shall have the effects for purposes of this subsection of an application filed in the United States only if the international application designated the United States and was published under Article 21(2) of such treaty in the English language.

Claims 1-2, 6, 8-13, 15, 18-20, 22-27, 31 and 33 are rejected under 35 U.S.C. 102(e) as being anticipated by Sugimura, et al. (US 6136743).

Sugimura, et al. teach a method of making and using a supported ('fine particulate carrier") metallocene polyolefin catalyst. The process method taught includes the steps of

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providing particulate catalyst support material (col. 26, l. 28-32; col. 49, l. 63 – col. 50, l. 31) an alumoxane co-catalyst (col. 42, l. 30 – col. 43, l. 4) in hydrocarbon solvent (col. 43, l. 5-27) providing a dispersion with a metallocene having two sterically dissimilar cyclopentadienyl rings coordinated in a stereorigid orientation with a central transition metal to prevent ring rotation (col. 5, l. 38 – col. 6, l. 36; col. 7, l. 50 – col. 8, l. 67; col. 11, l. 64 – col. 17, l. 15; col. 17, l. 25 – col. 20, l. 16) mixing metallocene solvent dispersion and alumoxane (col. 50, l. 33 – col. 51, l. 32) at a temperature of about 10 °C or less then recovering and washing with paraffinic hydrocarbon solvent at a temperature of about 10 °C or less (col. 53, l. 13-20) and dispersing within mineral oil with greater viscosity than paraffinic hydrocarbon solvent (col. 53, l. 21-25; col. 56, l. 27-29). Desired ratios of aluminum to transition metal, organometallic compound to transition metal compound are taught (col. 57, l. 13-35).

Double Patenting

The nonstatutory double patenting rejection is based on a judicially created doctrine grounded in public policy (a policy reflected in the statute) so as to prevent the unjustified or improper timewise extension of the "right to exclude" granted by a patent and to prevent possible harassment by multiple assignees. See *In re Goodman*, 11 F.3d 1046, 29 USPQ2d 2010 (Fed. Cir. 1993); *In re Longi*, 759 F.2d 887, 225 USPQ 645 (Fed. Cir. 1985); *In re Van Ornum*, 686 F.2d 937, 214 USPQ 761 (CCPA 1982); *In re Vogel*, 422 F.2d 438, 164 USPQ 619 (CCPA 1970);and, *In re Thorington*, 418 F.2d 528, 163 USPQ 644 (CCPA 1969).

A timely filed terminal disclaimer in compliance with 37 CFR 1.321(c) may be used to overcome an actual or provisional rejection based on a nonstatutory double patenting ground provided the conflicting application or patent is shown to be commonly owned with this application. See 37 CFR 1.130(b).

Effective January 1, 1994, a registered attorney or agent of record may sign a terminal disclaimer. A terminal disclaimer signed by the assignee must fully comply with 37 CFR 3.73(b).

Claims 1-34 are rejected under the judicially created doctrine of obviousness-type double patenting as being unpatentable over claims 1-14 of **US 6,239,058**. Although the conflicting claims are not identical, they are not patentably distinct from each other because both patent and instant application claim a process for making a metallocene catalyst which is

400 Å.

supported on silica where said support is treated with alumoxane and the metallocene catalyst

has two cyclopentadienyl rings, capable of forming fluorenyl rings, said cyclopentadienyl rings

can be the same or different, substituted or unsubstituted, bridged or non bridged, so that a

different symmetry is assigned to each of the rings. The metal compound may be zirconium or

any group IVB metal. Non polar solvent used was toluene.

Instant application claims silica particles are impregnated with alumoxane co-catalyst such that the alumoxane is retained primarily on the surface of the silica particles, that the temperature for impregnation and subsequent washing steps are at 10 °C or less, and that washed catalyst is dispersed in a viscous mineral oil. Furthermore silica particle size range is between 20-60 microns, weight ratio of alumoxane to silica is 0.6-2.0, weight ratio of metallocene to support ratio is 0.1-6.0 weight percent and pore diameter ranges between 200-

It would have been obvious to one of ordinary skill in the art to have modified the catalyst preparation process as described in the patent such that the alumoxane contribution is determined as amount of surface area of silica because it is solubilized and would therefore be accessible to the surface of silica because the surface inherently would be open to accept liquid and considering the particle size range and weight ratio of alumoxane to silica are similar as are the weight ratio of metallocene to support, it would be obvious that surface area is an inherent property of the silica support and the solubility of alumoxane dispersed in solution would more accurately determine the amount which is found on the surface area of the silica support when dried which would be dependent upon temperature at which the reaction is carried out which is known in the art and it is also known to disperse catalyst components in an inert liquid carrier

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because it can be introduced into a reactor in a manner where it will not react with the reactor walls.

Claims 1-34 are rejected under the judicially created doctrine of obviousness-type double patenting as being unpatentable over claims 1-17 of **US 6,166,153**. Although the conflicting claims are not identical, they are not patentably distinct from each other because both patent and instant application claim a process for making a metallocene catalyst which is supported on silica where said support is treated with alumoxane and the metallocene catalyst has two cyclopentadienyl rings, capable of forming fluorenyl rings, said cyclopentadienyl rings can be the same or different, substituted or unsubstituted, bridged or non bridged, so that a different symmetry is assigned to each of the rings. The metal compound may be zirconium or any group IVB metal. Inert liquid carrier used is mineral oil.

Instant application claims silica particles are impregnated with alumoxane co-catalyst such that the alumoxane is retained primarily on the surface of the silica particles, that the temperature for impregnation and subsequent washing steps are at 10 °C or less, and that washed catalyst is dispersed in a viscous mineral oil. Furthermore silica particle size range is between 20-60 microns, weight ratio of alumoxane to silica is 0.6-2.0, weight ratio of metallocene to support ratio is 0.1-6.0 weight percent and pore diameter ranges between 200-400 Å.

It would have been obvious to one of ordinary skill in the art to have modified the catalyst preparation process as described in the patent such that the alumoxane contribution is determined as amount of surface area of silica because it is solubilized and would therefore be accessible to the surface of silica because the surface inherently would be open to accept liquid

and considering the particle size range and weight ratio of alumoxane to silica are similar as are the weight ratio of metallocene to support, it would be obvious that surface area is an inherent property of the silica support and the solubility of alumoxane dispersed in solution would more accurately determine the amount which is found on the surface area of the silica support when dried which would be dependent upon temperature at which the reaction is carried out which is known in the art and it is also known to disperse catalyst components in an inert liquid carrier because it can be introduced into a reactor in a manner where it will not react with the reactor walls.

Claims 1-31 are rejected under the judicially created doctrine of obviousness-type double patenting as being unpatentable over claims 1-20 of **US 5,968,864**. Although the conflicting claims are not identical, they are not patentably distinct from each other because both patent and instant application claim a process for making a metallocene catalyst which is supported on silica where said support is treated with alumoxane in a non polar solvent at a temperature of –20 to 0 °C and the metallocene catalyst has two cyclopentadienyl rings, capable of forming indenyl rings, capable of forming fluorenyl rings, said cyclopentadienyl rings can be the same or different, substituted or unsubstituted, bridged or non bridged, so that a different symmetry is assigned to each of the rings. The metal compound may be zirconium or any group IVB metal in a non polar solvent. Silica used has a surface area in the range from 200 to 800 m²/g and average pore volume from 0.70 ml/g to 1.6 ml/g and average particle size from 15 to 38 microns.

Instant application claims silica particles are impregnated with alumoxane co-catalyst such that the alumoxane is retained primarily on the surface of the silica particles, that the

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temperature for impregnation and subsequent washing steps are at 10 °C or less, and that washed catalyst is dispersed in a viscous mineral oil. Furthermore silica particle size range is between 20-60 microns, weight ratio of alumoxane to silica is 0.6-2.0, weight ratio of metallocene to support ratio is 0.1-6.0 weight percent and pore diameter ranges between 200-400 Å.

It would have been obvious to one of ordinary skill in the art to have modified the catalyst preparation process as described in the patent such that the alumoxane contribution is determined as amount within the pore structure of silica because it is solubilized and would therefore be accessible to the pore structure of silica because the pores inherently would be open to accept liquid and considering the particle size range and weight ratio of alumoxane to silica are similar as are the weight ratio of metallocene to support, it would be obvious that pore size is an inherent property of the silica support and the solubility of alumoxane in solution would more accurately determine the amount which is found in the pores of the silica support when dried which would be dependent upon temperature at which the reaction is carried out which is known in the art.

Claims 1-31 are rejected under the judicially created doctrine of obviousness-type double patenting as being unpatentable over claims 1-16 of **US 6,432,860**. Although the conflicting claims are not identical, they are not patentably distinct from each other because both patent and instant application claim a process for making a metallocene catalyst which is supported on silica where said support is treated with alumoxane in a non polar solvent so that the support pores have residual co-catalyst within the pores where 50% of the alumoxane is within the pores will then contact with the metallocene catalyst which has two cyclopentadienyl

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rings in a stereorigid relationship to the transition metal and 90 weight % of the metallocene supported on the particulate support is contained within the pore volume of the support. Silica used has an average pore volume from 1.2 ml/g to 1.5 ml/g and average spheroidal particle size from 10 to 40 microns.

Instant application claims silica particles are impregnated with alumoxane co-catalyst such that the alumoxane is retained primarily on the surface of the silica particles, that the temperature for impregnation and subsequent washing steps are at 10 °C or less, and that washed catalyst is dispersed in a viscous mineral oil. Furthermore silica particle size range is between 20-60 microns, weight ratio of alumoxane to silica is 0.6-2.0, weight ratio of metallocene to support ratio is 0.1-6.0 weight percent and pore diameter ranges between 200-400 Å.

It would have been obvious to one of ordinary skill in the art to have modified the catalyst preparation process as described in the patent such that the alumoxane contribution is determined as amount within the pore structure of silica because it is solubilized and would therefore be accessible to the pore structure of silica because the pores inherently would be open to accept liquid and considering the particle size range and weight ratio of alumoxane to silica are similar as are the weight ratio of metallocene to support, it would be obvious that pore size is an inherent property of the silica support and the solubility of alumoxane in solution would more accurately determine the amount which is found in the pores of the silica support when dried which would be dependent upon temperature at which the reaction is carried out which is known in the art and pore structure is incorporated into calculations when using surface area calculations.

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Claims 1-31 are provisionally rejected under 35 U.S.C. 101 as claiming the same invention as that of claims 1-34 of copending Application No. 09/782,753. This is a <u>provisional</u> double patenting rejection since the conflicting claims have not in fact been patented.

Both applications are drawn to a process for the preparation of a supported metallocene catalyst where a particulate silica alumoxane support is mixed with a metallocene catalyst in an aromatic hydrocarbon solvent, mixed at a temperature of about 10 °C or less, recovering supported catalyst from solvent, washing in a paraffinic hydrocarbon solvent at a temperature of about 10 °C or less and dispersing washed catalyst in hydrocarbon solvent which is mineral oil. Both applications claim a supported catalyst value of no more than 50% by weight, mineral oil viscosity of at least 10 centistokes and paraffinic hydrocarbon solvent viscosity of no more than 2 centistokes, optional subsequent washing step, silica average particle size overlap between 20-50 microns, different stereospecificity between cyclopentadienyl structures, an identical syndiospecific metallocene formula having substituted or unsubstituted fluorenyl groups, metals which are titanium, zirconium, hafnium or vanadium, R" is methylene, ethylene, organosilyl, substituted methylene or substituted ethylene radical, (Cp_aR_n) fluorenyl radical has bilaterial symmetry and R' is selected such that (Cp_bR'_m) forms an alkyl substituted or unsubstituted cyclopentadiencyl radical having bilateral symmetry, weight ratio alumoxane to silica overlaps from 0.6 to 1.5, both claim a isopropylidene (cyclopentadienyl-1-2,7-di-tert-butyl fluorenyl) ligand or a diphenyl methylene (cyclopentadienyl-1-fluorenyl) ligand, both claim an identical isospecific metallocene which is inherently stereorigid if there is a bridging ligand between the cyclopentadienyl ligands where the indenyl groups are substituted or unsubstituted at the proximal position and selected from racemic dimethylsilyl(2-methyl-4-phenyl indenyl),

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zirconium dichloride, racemic dimethylsilyl(2-methyl-4-indenyl)₂ zirconium dichloride, and racemic dimethylsilyl(2-methyl-4,5-benzo indenyl)₂ zirconium dichloride and mixtures thereof.

Any inquiry concerning this communication or earlier communications from the examiner should be directed to Jennine M. Brown whose telephone number is (703) 305-0435. The examiner can normally be reached on M-F 8:00 AM - 4:30 PM.

If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Mark Bell can be reached on (703) 308-3823. The fax phone numbers for the organization where this application or proceeding is assigned are (703) 879-9310 for regular communications and (703) 872-9311 for After Final communications.

Any inquiry of a general nature or relating to the status of this application or proceeding should be directed to the receptionist whose telephone number is (703) 308-0661.

jmb May 5, 2003

> Supervisory Patent Examiner Technology Center 1700